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CORRIGENDUM

'Gas diffusion from ascending gas bubbles',
by PAUL H. LEBLOND, *J. Fluid Mech.* vol. **35**, 1969, p. 711.

As was pointed out to me by T. R. Hennessy of the University of Cape Town, the expressions F_c and F_d appearing at the bottom of p. 715 should be divided by 4π, and the factor $r^{\frac{4}{3}}$ removed from the latter. The coefficients β_c and β_d on p. 716 should then be divided by 4π. Equations (9*a*) and (10*a*) are unchanged but (9*b*) and (10*b*) become

$$\frac{dr}{dP} = -\left[\beta_d(P-\gamma) - \frac{2\alpha g r^3}{9\nu}\right] \Big/ \frac{2\sigma}{r^2}\left[\beta_d(P-\gamma) - \frac{2\alpha g}{9\nu}\frac{3P}{2\sigma}r^4\right], \tag{9b}$$

$$r_a(P) = \left[\frac{9\nu\beta_d}{2\alpha g}(P-\gamma)\right]^{\frac{1}{3}}, \quad r_b(P) = \left(\frac{2\sigma_i}{3P}\right)^{\frac{1}{4}}[r_a(P)]^{\frac{3}{4}}, \tag{10b}$$

and the ratio r_b/r_a for a dirty bubble is now $(2\sigma/3Pr_a)^{\frac{1}{4}}$. The values of table 1 should be modified as follows: for a clean system, r_a should be multiplied by 0·364, r_b by 0·485; for the contaminated system, $r_a = 0{\cdot}428$ (r_a of table 1)$^{\frac{5}{9}}$, $r_b = 0{\cdot}528$ (r_b of table 1)$^{\frac{8}{9}}$. The other results of the paper are unchanged.